A First Course on Kinetics and Reaction Engineering

Class 2 on Unit 2



Where We've Been

- Part I Chemical Reactions
 - ▶ 1. Stoichiometry and Reaction Progress
 - ▶ 2. Reaction Thermochemistry
 - Numerical Solution of Non-Linear Equations (Supplemental Unit S2)
 - 3. Reaction Equilibrium
- Part II Chemical Reaction Kinetics
- Part III Chemical Reaction Engineering
- Part IV Non-Ideal Reactions and Reactors



Reaction Thermochemistry

- Heat of reaction at 298 K
 - Using heats of formation at 298 K

-
$$\Delta H_{j}^{0}(298 \text{ K}) = \sum_{i=\text{all}} v_{i,j} \Delta H_{f,i}^{0}(298 \text{ K})$$

Using heats of combustion at 298 K

-
$$\Delta H_{j}^{0}(298 \text{ K}) = \sum_{\substack{i=\text{all} \\ \text{species}}} v_{i,j}(-\Delta H_{c,i}^{0}(298 \text{ K}))$$

- Heat of reaction at other temperatures
 - ▶ If there are no phase changes between 298 K and the temperature of interest

$$- \Delta H_{j}^{0}(T) = \Delta H_{j}^{0}(298 \text{ K}) + \sum_{\substack{i = \text{all} \\ \text{species}}} \left(v_{i,j} \int_{298K}^{T} \hat{C}_{p,i} dT \right)$$

Gibbs free energy change for reaction at 298 K

$$\Delta G_{j}^{0}(298 \text{ K}) = \sum_{\substack{i=\text{all} \\ \text{species}}} v_{i,j} \Delta G_{f,i}^{0}(298 \text{ K})$$

- Adiabatic temperature change
 - ▶ If there are no phase changes between initial and final temperatures, T₁ and T₂

$$-\sum_{j=1}^{N_{ind}} \xi_j \left(-\Delta H_j \left(T_1 \right) \right) = \sum_{\substack{i=all \ species}} \int_{T_1}^{T_2} \hat{C}_{p,i} \left(n_i^0 + V_{i,j} \xi_j \right) dT$$



Questions?



Calculation of Heats of Reaction

- This activity will use the 02_Activity_1_Handout.pdf file; please take it out
- The handout is a solution to a problem
 - ▶ It presents the calculation of the heat of the water-gas shift reaction at 250 °C
 - It contains one or more mistakes
- Identify as many errors as you can in the next ~5 minutes



Calculation of Heats of Reaction

- This activity will use the 02_Activity_1_Handout.pdf file; please take it out
- The handout is a solution to a problem
 - It presents the calculation of the heat of the water-gas shift reaction at 250 °C
 - It contains one or more mistakes
- Identify as many errors as you can in the next ~5 minutes
 - You can't arbitrarily mix heats of formation and combustion; the calculated heat at 298K is wrong.
 - The heat calculated in the solution is for C + CO + O₂ + H₂O → 2 CO₂ + H₂ (if the correct values of the stoichiometric coefficients are used)
 - ▶ While the proper sign convention was used, the calculation used the starting moles of reactants and final moles of products where it should have used stoichiometric coefficients.
 - ► The calculation failed to account for the latent heat of vaporization of water upon heating from 298 to 543 K
 - There may be a problem with the heat capacities: it seems odd that hydrogen is nearly equal to the carbon oxides
 - Actually, the values are bad because the calculation took the first term of a polynomial expression and ignored the temperature dependent terms (you wouldn't be expected to catch this just by looking at the calculation)
- Consider how to correct the solution
 - What equations would you use?
 - What additional data would you need, beyond what was provided?



Common Ways to Correct the Mistakes

Calculation of the heat of reaction at 298 K

• Use heats of combustion
$$\Delta H_1^0(298 \text{ K}) = v_{CO,1}(-\Delta H_{c,CO}^0(298 \text{ K})) + v_{CO_2,1}(-\Delta H_{c,CO_2}^0(298 \text{ K}))$$

- with liquid water as the product
- with hypothetical ideal gas water as the product

• Use heat of formation
$$\Delta H_1^0(298 \text{ K}) = v_{CO,1}(\Delta H_{f,CO}^0(298 \text{ K})) + v_{CO,1}(\Delta H_{f,CO_2}^0(298 \text{ K}))$$

- with same two standard states

$$+v_{H_2O,1}\left(\Delta H_{f,H_2O_{(I)}}^0(298 \text{ K})\right)+v_{H_2,1}\left(\Delta H_{f,H_2}^0(298 \text{ K})\right)$$

 $+v_{H_2O,1}\left(-\Delta H_{c,H_2O_{(I)}}^0(298 \text{ K})\right)+v_{H_2,1}\left(-\Delta H_{c,H_2}^0(298 \text{ K})\right)$

Calculation of the heat of reaction at 543 K

$$\Delta H_1^0 (543 \text{ K}) = \Delta H_1^0 (298 \text{ K}) + v_{CO,1} \int_{298 \text{ K}}^{543 \text{ K}} \hat{C}_{p,CO} dT + v_{CO_2,1} \int_{298 \text{ K}}^{543 \text{ K}} \hat{C}_{p,CO_2} dT + v_{H_2,1} \int_{298 \text{ K}}^{543 \text{ K}} \hat{C}_{p,H_2} dT +$$

If liquid water was the standard state

$$v_{H_2O,1} \left[\int_{298 \text{ K}}^{373 \text{ K}} \hat{C}_{p,H_2O_{(I)}} dT + \Delta H_{v,H_2O}^0 (373 \text{ K}) + \int_{373 \text{ K}}^{543 \text{ K}} \hat{C}_{p,H_2O_{(v)}} dT \right]$$

If ideal gas water was the standard state

$$v_{H_2O,1} \int_{298 \text{ K}}^{543 \text{ K}} \hat{C}_{p,H_2O_{(v)}} dT$$

 It is essential to identify one standard state for each species and then to use that standard state consistently throughout the problem solution



Solving Algebraic Equations

Representation of the equations:
$$\begin{cases} 0 = f_1(z_1, z_2, \dots, z_n) \\ 0 = f_2(z_1, z_2, \dots, z_n) \\ \vdots \\ 0 = f_n(z_1, z_2, \dots, z_n) \end{cases}$$

$$\vdots \\ 0 = f_n(z_1, z_2, \dots, z_n)$$

• or in vector form:
$$0 = \underline{f}(\underline{z})$$

- General approach
 - Guess the solution, z_0 , use the guess to generate approximate linear equations, solve the approximate linear equations to obtain an improved guess
 - Repeat that process until
 - A specified number of iterations have occurred
 - A specified number of function evaluations have occurred
 - The values of the functions less than some specified tolerance
 - The values of the unknowns are changing by less than some specified tolerance
- The equations can be linearized by truncating a Taylor series expansion

$$f_1(z_1, z_2, \dots, z_n) \simeq f_1(\underline{z_0}) + \frac{\partial f_1}{\partial z_1} \bigg|_{\underline{z_0}} (z_1 - (z_1)_0) + \frac{\partial f_1}{\partial z_2} \bigg|_{\underline{z_0}} (z_2 - (z_2)_0) + \dots + \frac{\partial f_1}{\partial z_n} \bigg|_{\underline{z_0}} (z_n - (z_n)_0)$$

The derivatives in the linearized equation can be approximated numerically

$$- \frac{\partial f_i}{\partial z_j}\bigg|_{z_0} \simeq \frac{f_i\Big(\big(z_1\big)_0, \cdots, \big(\big(z_j\big)_0 + \delta z_j\big), \cdots, \big(z_n\big)_0\Big) - i\Big(\big(z_1\big)_0, \cdots, \big(z_j\big)_0, \cdots, \big(z_n\big)_0\Big)}{\delta z_j}$$



Solving Algebraic Equations Using MATLAB

- The built-in MATLAB function fsolve performs the tasks just described
 - The user provides
 - a guess for the solution, **z**₀
 - a function that fsolve can call
 - this function takes values of the unknowns, z, as its only argument
 - it returns the values of the functions, \underline{f} , calculated using the values of \underline{z} passed to it
- A MATLAB template file named SolvNonDif.m is provided for your use
 - It requires four modifications
 - Enter the values of any constants that appear in the problem being solved
 - Enter expressions to evaluate the functions, *f*, given the values of the variables, *z*
 - Enter the values to be used as the guess for the solution, **z**₀
 - Enter code to calculate any additional quantities that are desired using the solution to the equations
 - It produces
 - A message stating whether a valid solution was obtained
 - A solution, <u>z</u>, to the equations
 - The values of the functions, <u>f</u>, evaluated using the returned solution, <u>z</u>
 - A listing of the values of any additional quantities you entered code for
 - Step-by-step instructions for using it are provided
 - Example 1 illustrates its use



Problem Statement

In equations (1) through (4) A, B and C are constants with values of 0.2083 mol/min, 5.472 min/mol and 0.4164 mol/min, respectively. Solve the equations for z_1 , z_2 , z_3 and z_4 , and then compute the ratio of z_1 to z_2 .

$$f_1(\underline{z}) = A - Bz_1^{1.5}z_2^{0.5} - z_1 = 0 \tag{1}$$

$$f_2(\underline{z}) = C - Bz_1^{1.5} z_2^{0.5} - z_2 = 0$$
 (2)

$$f_3(\underline{z}) = Bz_1^{1.5}z_2^{0.5} - z_3 = 0 \tag{3}$$

$$f_4(\underline{z}) = Bz_1^{1.5}z_2^{0.5} - z_4 = 0 \tag{4}$$

- The equations do not contain derivatives or integrals, only algebraic terms
 - SolvNonDif.m can be used to solve the equations
 - Follow the step-by-step instructions provided with this supplemental unit
- Save a copy of SolvNonDif.m as S2_Example_1.m
 - Modify the initial comment
 - Change the function declaration statement
 - It will require four modifications before it can be used
 - A copy of the fully-modified file is included with this supplemental unit



First Modification of SolvNonDif.m.

- First required modification: define variables to hold the values of all constants that appear in the problem being solved
 - Here there are three: A, B and C
 - Results of modification

```
% Modified version of the MATLAB template file SolvNonDif.m used to solve
% Example 1 of Supplemental Unit S2 of "A First Course on Kinetics and
% Reaction Engineering."
%
function z = S2_Example_1
% Known quantities and constants (in units of mol and min)
A = 0.2083;
B = 5.472;
C = 0.4167;
```



Second Modification of SolvNonDif.m

 Provide code to evaluate the functions, f, within the internal function evalEqns

$$f_{1}(\underline{z}) = A - Bz_{1}^{1.5}z_{2}^{0.5} - z_{1} = 0$$

$$f_{2}(\underline{z}) = C - Bz_{1}^{1.5}z_{2}^{0.5} - z_{2} = 0$$

$$f_{3}(\underline{z}) = Bz_{1}^{1.5}z_{2}^{0.5} - z_{3} = 0$$

$$f_{4}(\underline{z}) = Bz_{1}^{1.5}z_{2}^{0.5} - z_{4} = 0$$

Resulting modification

```
% Function that evaluates the equations
function f = evalEqns(z)

term1 = z(1)^1.5*z(2)^0.5;

f = [
    A - B*term1 - z(1);
    C - B*term1 - z(2);
    B*term1 - z(3);
    B*term1 - z(4);
];
end % of internal function evalEqns
```



Third and Fourth Modifications of SolvNonDif.m

- Third modification is to provide guesses for the solution
- Fourth (and final modification) is to calculate additional desired or requested quantities using the solution
 - ▶ Here we are asked for the ratio of z₁ to z₂



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